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PATENT ABSTRACTS OF JAPAN, unexamined applications, C field, vol. 7, No. 155
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DIE PHARMAZIE, vol. 39, No. 6, 1984, Berlin E.
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Description

This invention relates to therapeutic compositions with controlled release of medicaments in which particles of non-ionic polymer which is insoluble but swellable in water are loaded with the medicament and coated with a Polymer film, and to their preparation process.

State of the art

Orally administered medicaments are often poorly absorbed, with consequent very low hematic levels. This problem is accentuated when prolonged release over twelve or even twentyfour hours is required. In this respect, with known pharmaceutical controlled release forms, poorly soluble medicaments normally give rise to hematic levels which in many cases are not even therapeutically valid.

Patent AU-A-8,770,043 describes dispersions or solutions of dihydropyridine derivatives (water-insoluble) in semisolid or liquid non-ionic surfactants. These dispersions result in improved bioavailability. The controlled release is obtained by inserting the dispersions into gelling matrices based on hydrophilic polymers such as hydroxypropylmethylcellulose.

Patent GB-A-2,159,714 describes steroid medicaments with a water solubility of less than one part in 5000 by weight, which are sprayed onto inert cores in the form of suspensions in solutions of water-soluble polymer binders. Successive polymer films of controlled release type are then applied to these cores loaded with the medicament. The improvement in absorption is obtained by micronizing the medicament particles and introducing surface-active wetting agents into the suspension to be sprayed.

Patents DE-A-2,643,004, DE-A-3,320,583 and EP-A-78,430 describe the loading of poorly soluble medicaments onto crosslinked polyvinylpyrrolidone by a method comprising swelling in solvent.

Patent GB-A-2,153,676 describes the loading of the medicament onto crosslinked polyvinylpyrrolidone by a process involving heating the medicament and crosslinked polymer mixture. Patent GB-A-2,153,678 attains the same result by a process involving co-grinding the mixture of medicament and crosslinked polymer in a high-energy mill.

The present applicant (see Italian patent applications IT 22336 A/88 and IT 22770 A/88) has proposed a further two methods for activating poorly soluble medicaments on crosslinked hydrophilic polymers which are insoluble but swellable in water.

All the described patents enable systems comprising medicaments supported on hydrophilic crosslinked polymers to be obtained having a very high solubility or dissolution rate but a very short medicament release time.

Patent SA-A-870,738 (corresponding to EP-A-232,155) describes a system in which the crosslinked polyvinylpyrrolidone is loaded with a solution of the medicament and linear polyvinylpyrrolidone, the loaded product then being mixed with a gelling polymer. The mixture can be granulated or pressed after adding any other excipients.

Patent BE-A-729,827 describes systems consisting of particles or granules of ion exchange resins of size between 0.1 and 1 mm loaded with ionic medicaments and coated with impermeable polymers by coating in a pan.

Patents US-A-4,221,778 and EP-A-171,528 describe particles of ion exchange resin loaded with ionic medicaments which are pretreated with substances such as polyethyleneglycols or glycerin before coating with polymer films in a fluidized bed.

Patent EP-A-294,103 describes a method in which the ion exchange resins are coated by dispersing the polymer particles (between 5 and 1000 nm) in solutions of the coating polymer, followed by phase separation or spray drying.

Finally, patent US-A-4,795,644 describes ion exchange resin particles on which a polymer film containing water-soluble substances such as alkaline metal salts or sugars able to form pores is deposited.

It is apparent that in the foregoing systems the achievement of controlled release is based on the synergic effect between the action of the polymer membrane deposited on the polymer microparticles and the ionic interaction between the resin and the medicament.

Further examples of controlled release therapeutic compositions wherein core substances are coated with polymeric materials can be found in the following documents:

- Jp-Kokai N. 58-67 616 (Patent Abstract of Japan) relates to quick enteric release microcapsules having a wall membrane formed by ethylcellulose mixed with a polysaccharide. The addition of a water-swelling polymers to the microcapsule core is said to accelerate the enteric release.
- EP-A-250,374 describes coated mini-units. The core is obtained by compressing a mixture of the active ingredient with water-swelling polymers; the polymeric coating controls the release by means of

an osmotic mechanism.

- EP-A-147,780 describes compositions comprising core tablets or granules wherein the drug is blended with microcrystalline cellulose and other excipients, and a polyvinyl alcohol coating.

It is worth noting that in the above examples the cores to be coated are obtained simply by admixing or blending the active ingredients with the polymers.

- EP-A-347,748 describes granules containing the active ingredient and polymers such as povidone, coated with a mixture of microcrystalline cellulose and povidone or cellulose derivatives.

In this case, the polymeric coating has just enhancing-compression properties.

In other compositions no coating is required to achieve the controlled release, which is exclusively related to the properties of the drug matrix, as in the case of EP-A-293, 537, which describes sustained release inclusion complexes of various drugs with hydrophobic cyclodextrine derivatives, and of GB-A-2,202,143, relating to drugs dispersed in a microcrystalline cellulose matrix containing small amount of cellulose derivatives.

None of the above discussed prior art documents teaches or suggests that prolonged release compositions can be obtained from the short release medicaments supported on hydrophilic cross-linked polymers cited before.

Detailed description of the invention

In contrast to that reported in the aforesaid state of the art, it has been unexpectedly found that the release of medicaments loaded onto particles of non-ionic polymer which is insoluble but swellable in water can be prolonged even for many hours if said medicament-loaded particles are coated with linear polymer delay films.

The present invention therefore provides systems for the controlled release of medicaments supported on crosslinked polymers and coated with polymer films, their preparation process and the pharmaceutical compositions which contain them.

The process for preparing the systems of the present invention consists essentially of the following steps:

- 1) loading the particles of water-insoluble but water-swellable polymer with the required medicament either by swelling with solutions of the medicament followed by drying, or by high-energy co-grinding;
- 2) suspending such loaded polymer particles, of between 1 and 200 μm , in a current of air in a fluidized bed apparatus, spraying them with a solution of the coating polymer, and then drying them in the same apparatus or by another method;
- 3) size-enlarging the medicament-loaded polymer particles by wet or dry granulation to a homogeneous size of between 100 and 1000 μm and then coating them as described under point 2.

The size of the coated polymer particles is between the limits of 10-1500 μm and preferably 100-1000 μm .

The medicament release system obtained in this manner has a medicament release time which can be adjusted at will from a few hours to 24-48 hours. The medicament loaded onto the polymer particles is in a thermodynamically active state, ie amorphous or as extremely small crystals (nanocrystals).

The process according to the invention is implemented in two stages as follows:

1st Stage

The medicament is loaded onto the particles of crosslinked polymer insoluble but swellable in water (or onto a mixture of two or more such polymers) by any known method, such as:

- 1a) dissolving the medicament in a suitable solvent and spraying a certain volume of the solution onto a given quantity of polymer with the weight ratio of solution to polymer chosen on the basis of the polymer swelling capacity and the medicament concentration in the solution. The spraying can be carried out in any apparatus used for the purpose, such as a continuously stirred reactor, a rotary evaporator under continuous rotation, a mortar by light mixing with a pestle, or a fluidized bed with the polymer kept suspended in an air stream.

The product obtained is then dried in the above apparatus or in other suitable apparatus.

- 1b) the medicament is dissolved in a suitable solvent and a quantity of a crosslinked polymer insoluble but swellable in water (or a mixture of two or more such polymers) is suspended in an excess of the solution obtained. The suspension is kept stirring until the polymer particles have swollen. The suspension is then filtered or separated by other suitable means, and the product recovered and dried.

1c) the medicament in powder form and the crosslinked polymer insoluble but swellable in water (or a mixture of two or more such polymers), also in powder form, are homogeneously mixed together and then co-ground in a suitable apparatus such as a ball mill, a high-energy vibration mill, an air jet mill etc.

1d) the medicament in powder form and the crosslinked polymer insoluble but swellable in water (or two or more such polymers), also in powder form, are homogeneously mixed together and then co-ground in a suitable apparatus in which the grinding chamber is saturated with solvent vapour or is subjected to a stream of solvent vapour, the solvent being chosen from those able to swell the polymer. The co-grinding is carried out for example in a ball mill, a high-energy vibration mill or a hammer mill, in which the grinding chamber is connected via a valve and pipe to a solvent reservoir.

1e) the medicament in powder form and the crosslinked polymer insoluble but swellable in water, also in powder form, are mixed together homogeneously and then co-heated to the medicament melting point in an apparatus such as an oven, rotary evaporator, reaction vessel, oil bath etc, until the medicament has melted and has been absorbed by the polymer.

The weight ratio of the medicament to said polymer or polymer mixture is in all cases between 0.1 and 1000 parts by weight of medicament per 100 parts by weight of polymer, and preferably between 10 and 100 parts by weight of medicament per 100 parts by weight of polymer.

2nd Stage

When the polymer has been loaded with the active principle, the powder is directly coated with polymer film. Alternatively the polymer film coating can be applied not directly to the medicament-loaded polymer powder but to granules (or pellets) obtained by a size enlargement process carried out on either the starting powder alone or on a mixture of said powder with suitable excipients.

Non-limiting examples of such size enlargement processes are:

- dry granulation, based on pressing the loaded polymer powder or its mixture with suitable excipients, followed by crumbling and screening to the desired size;
- wet granulation, based on wetting the loaded polymer powder or its mixture with suitable excipients with an aqueous or solvent solution of binders such as sugars, linear polymers etc. in an arm, sigma or other mixer, then wet-screening the paste, drying the resultant aggregates in a forced-air static dryer or in suspension in a fluidized air bed, then crumbling and screening to the desired size;
- rapid wet granulation, based on a process of wetting, kneading and sizing the aggregates in apparatus with high speed homogenization systems, then drying and screening;
- wet granulation as heretofore described, followed by extrusion and spherodization to improve the morphology of the granules to be coated, then drying and screening.

When the medicament-loaded polymer powder or its granulate has been obtained, it is coated by suspending a weighed quantity of the powder or granulate in a hot air stream within the drum of a fluidized bed apparatus equipped with a Wurster insert and a binary nozzle. The air flow is such as to maintain a continuous change of suspended powder in the region in which the solution or suspension of coating polymer is sprayed. The polymer dispersion (or solution) is fed with a peristaltic pump. The quantity of filming agent sprayed per unit time and the total quantity, the atomization pressure, the nozzle size, the temperature and the air volume used in executing a cycle depend on the quantity, the dimensions of the product to be coated and the extent of the controlled release to be obtained. On termination of spraying, the product is dried directly in the fluidized bed or in a forced-air oven. If necessary, an anti-adhesion agent can be added to the product to ensure separation of the film-coated particles.

Examples of water-insoluble but water-swellable crosslinked polymers which can be used are:

- crosslinked polyvinylpyrrolidone (abbreviated to crospovidone), as described in National Formulary, Supplement 3, page 368;
- crosslinked sodium carboxymethylcellulose, as described in National Formulary, Supplement 3, page 367;
- crosslinked β -cyclodextrin polymer, as described in patent WO 83/00809 and by Fenylvest et al. in Pharmazie 39, 473, 1984;
- crosslinked dextran, etc.

Of particular interest is the use of crosslinked β -cyclodextrin polymer, which up to now has been used only as a disintegrator for solid pharmaceutical compositions and not as a support for medicaments, and the use of crospovidone.

It should however be noted that according to the present invention any polymer having the following characteristics can be used:

- a hydrophilic polymer lattice which results in considerable swellability in water
- water-insolubility by virtue of the nature of the polymer lattice. Non-limiting examples of linear polymers which can be deposited as coating films on the particles of crosslinked polymer previously loaded with the medicament are:
- 5 - cellulose and derivatives soluble or insoluble in aqueous solutions, such as: ethylcellulose, methylcellulose, hydroxypropylcellulose, hydroxypropylmethylcellulose, cellulose acetate, cellulose acetobutyrate, cellulose acetotrimellitate, cellulose acetophthalate etc.
- acrylic and methacrylic polymers and their copolymers soluble or insoluble in aqueous solutions such as: methacrylic acid-methylmethacrylate copolymer, ethylacrylate-methylmethacrylate copolymer,
- 10 - ethylacrylate-methylmethacrylate and trimethylammonium ethylmethacrylate chloride copolymer etc.
- linear polyvinylpyrrolidone of differing molecular weight, vinylpyrrolidone-vinyl acetate copolymer etc.
- polyanhydrides such as vinyl ether-maleic anhydride copolymer
- polyvinylalcohol.

It should however be noted that according to the present invention any polymer having the following characteristics can be used:

- insolubility at all pH values
- solubility only at determined pH values (eg. 4.5, 5.5, 6.0, 7.0)
- solubility at all pH values.

The aforesaid polymers can be used either alone or in mixture, with the addition of suitable plasticizers such as glycerin, polyethyleneglycols, citric acid esters, glycerin esters, phthalic acid esters etc.; of anti-adhesion substances such as talc, silica, magnesium stearate etc.; or of porogenic substances such as microcrystalline lactose, calcium carbonate, calcium phosphate, saccharose, sodium chloride, potassium chloride etc.

There are no particular limitations to the medicaments which can be used according to the present invention, and in fact either water-soluble medicament or medicaments poorly soluble in water can be used. Non-limiting examples of medicaments poorly soluble in water which can be used according to the present invention are: griseofulvin, indomethacin, diacerein, megestrol acetate, estradiol, progesterone, medroxyprogesterone acetate, nifedipine, nicergoline, paracetamol, clonidine, etoposide, lorazepam, temazepam, digoxin, glibenclamide, ketoprofen, indobufen, ibuprofen, diclofenac, naproxene, acemethacine etc.

In the case of water-soluble medicaments, the main advantage of the present invention is that their incorporation into the spherical particles of the water-insoluble crosslinked polymer facilitates the subsequent coating with polymer film. In this respect, in many cases the original morphology of said medicaments is very irregular (needles, very thin flakes etc.) and makes homogeneous and continuous coating of the particles over their entire surface difficult, with consequent poor control of the medicament release. In the particular case of insoluble medicaments in the form of weak acid salts of strong bases one advantage of the present invention is that their incorporation into the insoluble crosslinked polymer provides them with greater protection against the surrounding pH-variable environment in the different segments of the intestinal tract, this variable pH being able to influence the degree of ionization of the medicament and consequently its permeation characteristics. In order to control this ionization, the insoluble crosslinked polymer can also be loaded with agents able to suitably change the pH within the crosslinked polymer itself.

Non-limiting examples of water-soluble medicaments which can be used according to the present invention are: diltiazem hydrochloride, nicardipine hydrochloride, sodium chloride, captopril, enalapril, theophylline, ranitidine, verapamil hydrochloride, naproxene sodium salt, diclofenac sodium salt, propranolol, atenolol, sodium monofluorophosphate.

EXAMPLE 1

600 g of CROSPVIDONE (Kollidon CL, BASF) were loaded with 120 g of griseofulvin dissolved in 1.2 litres of methylenechloride in a chamber of a sigma mixer under continuous mixing. The thus swollen powder was dried in the same chamber at ambient temperature, at a residual pressure of 450-500 mbar; drying was completed in an oven under vacuum for 1 hour at 30 °C.

700 g of the powdered polymer loaded with griseofulvin in the aforesaid manner were mixed with 35 g of talc F.U. and 3.5 g of Aerosil'200 and were suspended in a 6" Wurster column of a GPCG1 fluidised bed plant and coated with 700 g of colloidal suspension of acrylic polymer EUDRAGIT RS 30D (ROEHM PHARMA) with added talc F.U., triethylcitrate plasticizer and Tween 80 surfactant under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 8-10 g/min. inlet air temperature 50 °C, product temperature 22-25 °C.

On termination of spraying, drying was carried out at the same inlet air temperature. The thus coated powder had the following percentage composition:

Griseofulvin	12.91
PVP CL	64.28
EUDRAGIT RS	8.11
TALC F.U.	12.68
CITROFLEX 2	1.63
TWEEN 80	0.01
SiO ₂	0.38
	<u>100.00</u>

EXAMPLE 2

120 g of griseofulvin dissolved in 1.2 litres of methylene chloride were loaded onto 600 g of crospovidone (Kollidon CL, BASF) kept under continuous mixing in a suitably sized sigma mixer. The thus swollen powder was dried in the same apparatus under vacuum (450-500 mbar of residual pressure) at ambient temperature. Drying was complete in an oven under vacuum for 1 hour at 30 °C.

700 g of the powdered polymer loaded with griseofulvin in the aforesaid manner were mixed with 35 g of talc F.U. and 3.5 g of Aerosil 200 and were suspended in a 6" Wurster column of a GPCG1 fluidised bed plant (GLATT, West Germany) and coated with 1050 g of colloidal suspension of acrylic polymer Eudragit RS 30D (ROEHM PHARMA) with added talc F.U. (anti-adhesion agent), triethylcitrate (plasticizer) and Tween 80 under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 8-10 g/min, air volume during process 2-3 m³/min, inlet air temperature 50 °C, product temperature 22-25 °C.

On termination of spraying, drying was carried out at the same inlet air temperature and volume. The thus coated powder had the following percentage composition:

Griseofulvin	11.77
PVP CL	58.67
EUDRAGIT RS	11.33
TALC F.U.	15.60
CITROFLEX 2	2.26
TWEEN 80	0.02
SiO ₂	0.35
	<u>100.00</u>

EXAMPLE 3

250 g of diacerein were activated by high-energy grinding with 250 g of povidone (Kollidon CL-M, BASF). 500 g of a mixture of excipients (30% lactose, 40% microcrystalline cellulose and 30% corn starch) were added to the 500 g of co-ground product and the resultant mixture was wet-granulated using a 5% solution of hydroxypropylcellulose in water as binder. The mixture was wet-screened and dried in a fluidized bed (GPCG1 Glatt, West Germany) under the following operating conditions: inlet air temperature 55 °C, inlet air volume 1-1.5 m³/min. The product was then dry-screened in an oscillating granulator. 2 g of granulate prepared as described were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 160 g of colloidal suspension of acrylic polymer Eudragit NE 30D (ROEHM PHARMA) with added talc F.U. (anti-adhesion agent), under the following operating conditions: atomisation pressure 1-1.5 bar, feed rate of coating suspension 2-3 g/min, inlet air temperature 30-40 °C, product temperature 25-30 °C, air volume during process 1.5-2 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. The thus coated granulate had the following percentage composition:

Diacerein	21.45
PVP CL	21.45
EUDRAGIT NE	8.80
LACTOSE	12.83
MICROCRYSTALLINE CELLULOSE	17.14
HYDROXYPROPYLCELLULOSE	2.20
CORN STARCH	12.83
TALC F.U.	3.30
	<u>100.00</u>

EXAMPLE 4

500 g of granulate obtained as described in Example 3 (particle size distribution 300-800 μm) were suspended in a 6" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 560 g of colloidal suspension of acrylic polymer Eudragit RS 30D (ROEHM PHARMA) with added talc F.U. (anti-adhesion agent), triethylcitrate (plasticizer) and Tween 80 under the following operating conditions: atomization pressure 1.5 bar, feed rate of coating suspension 10-12 g/min, air volume during process 2-3 m^3/min , inlet air temperature 50-60 °C, product temperature 30-35 °C. On termination of spraying, drying was carried out at the same inlet air temperature and volume. The thus coated granulate had the following percentage composition:

Diacerein	19.68
PVP CL	19.68
EUDRAGIT RS	12.09
LACTOSE	11.78
MICROCRYSTALLINE CELLULOSE	15.72
HYDROXYPROPYLCELLULOSE	2.01
CORN STARCH	11.78
TALC F.U.	4.83
TRIETHYLCITRATE	2.41
TWEEN 80	0.02
	<u>100.00</u>

EXAMPLE 5

200 g of granulate prepared as described in Example 3 were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 125 g of colloidal suspension of Eudragit RS 30D and Eudragit RL 30D acrylic polymer with added talc F.U. (anti-adhesion agent), triethylcitrate (plasticizer) and Tween 80 under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 2.5-5 g/min, inlet air temperature 55-60 °C, product temperature 30-32 °C, air volume during process 1-1.5 m^3/min . On termination of spraying, drying was carried out at the same inlet air temperature and volume. The thus coated granulate had the following percentage composition:

Diacerein	21.78
PVP CL	21.78
EUDRAGIT RS	3.35
EUDRAGIT RL	3.35
LACTOSE	13.04
CELLULOSE	17.41
HYDROXYPROPYLCELLULOSE	2.23
CORN STARCH	13.04
TALC F.U.	2.67
TRIETHYLCITRATE	1.34
TWEEN 80	0.01
	<u>100.00</u>

EXAMPLE 6

200 g of granulate prepared as described in Example 3 were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 1000 g of a 10% solution of Eudragit L100 acrylic polymer in a mixture composed of 6 parts of ethanol and 4 parts of deionized water with added talc F.U. (anti-adhesion agent) and n-dibutylphthalate (plasticizer) under the following operating conditions: atomization pressure 1 bar, feed rate of coating suspension 2-6 g/min, inlet air temperature 40-45 °C, product temperature 30-35 °C, air volume during process 1.5-2 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. The thus coated granulate had the following percentage composition:

Diacerein	14.78
PVP CL	14.78
EUDRAGIT L	30.30
LACTOSE	8.84
CELLULOSE	11.82
HYDROXYPROPYLCELLULOSE	1.52
CORN STARCH	8.84
TALC F.U.	3.04
N-DIBUTYLPHTHALATE	6.08
	<u>100.00</u>

EXAMPLE 7

45 g of nifedipine dissolved in 450 cc of methylene chloride were loaded onto 225 g of povidone (Kollidon CL-M, BASF) kept under constant stirring in a sigma mixer. After homogenization of the pasty mass the swelling solvent was extracted by a vacuum pump at a residual pressure of 450-500 mbar. After evaporation and recovery of the methylene chloride the loaded product was collected and drying completed in a vacuum oven (1 hour at 30 °C).

The 270 g of prepared product were returned to the mixing chamber of the sigma mixer and exposed to methylene chloride vapour for 24 hours. This operation was followed by drying in an oven, screening and homogenization by mixing the product. Colloidal silica (Aerosil 200, Degussa) was added to the final loaded product, which was then divided into flat tablets of 15 mm diameter weighing 500 mg and having a hardness of 7-10 Kp. These tablets were then reduced to granules with an oscillating granulator (or knife mill). The 425-1200 µm granulate fraction was removed by screening.

200 g of the granulate prepared as aforescribed were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 1330 g of a solution of Eudragit S100 acrylic polymer (ROEHM PHARMA) in ethanol/H₂O (80/20) with added talc F.U. (anti-adhesion agent) and n-dibutylphthalate (plasticizer) under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 3.5-5 g/min, inlet air temperature 38-40 °C, product temperature 30-32 °C, air volume during process 1.5-2.5 m³/min. On termination of spraying, drying was carried out at the same inlet

air temperature and volume. The thus coated granulate had the following percentage composition:

Nifedipine	10
PVP CL	50
COLLOIDAL SILICA	0.61
EUDRAGIT S	30.3
N-DIBUTYLPHTHALATE	3.03
TALC F.U.	6.06
	<u>100.00</u>

EXAMPLE 8

200 g of granulate prepared as described in Example 7 were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 833 g of colloidal suspension of Eudragit L30D acrylic polymer (ROEHM PHARMA) with added talc F.U. (anti-adhesion agent), n-dibutylphthalate (plasticizer) and Tween 80 under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 3-5 g/min, inlet air temperature 48-52 °C, product temperature 30-34 °C, air volume during process 1.5-2.5 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. The thus coated granulate had the following percentage composition:

Nifedipine	10
PVP CL	50
EUDRAGIT L30D	30.3
COLLOIDAL SILICA	0.61
N-DIBUTYLPHTHALATE	3.0
TALC F.U.	6.06
TWEEN 80	0.03
	<u>100.00</u>

EXAMPLE 9

200 g of granulate prepared as described in Example 7 were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 525 g of solution of Povidone (Kollidon 25, BASF) in ethanol with added talc F.U. (anti-adhesion agent) and glycerin (plasticizer) under the following operating conditions: spraying pressure 1 bar, feed rate of coating suspension 4.5-6 g/min, inlet air temperature 30-34 °C, product temperature 28-30 °C, air volume during process 1.5-2 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. 215 g of this coated granulate were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 285 g of colloidal suspension of ethylcellulose (Aquacoat ECD-30 FMC) with added talc F.U. (anti-adhesion agent), n-triethylcitrate (plasticizer) under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 3.5-5.5 g/min, inlet air temperature 50-55 °C, product temperature 30-35 °C, air volume during process 1.5-2 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. Percentage composition of final coated product:

Nifedipine	12.35
PVP CL	61.8
Colloidal silica	0.75
PVP K25	5.14
Glycerin	0.48
ETHYLCELLULOSE	14.98
TRIETHYLCITRATE	4.5
	<u>100.00</u>

EXAMPLE 10

215 g of granulate coated as described in the first part of Example 9 were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 285 g of colloidal suspension of ethylcellulose (Aquacoat ECD-30 FMC) with added hydroxypropyl methylcellulose (Methocel E5, Dow Chemical) and triethylcitrate (plasticizer) under the following operating conditions: atomization pressure 1-1.5 bar, feed rate of coating suspension 4-8 g/min, inlet air temperature 50-55 °C, product temperature 32-35 °C, air volume during process 1.5-2 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. The coated product was then discharged and 1% of powdered talc F.U. added, after which it was placed in an oven at a temperature of 60 °C for 2 hours. The thus coated granulate had the following percentage composition:

Nifedipine	12.35
PVP CL	61.75
Colloidal silica	0.75
PVP K25	5.14
GLYCERIN	0.71
HYDROXYPROPYLMETHYLCELLULOSE	3.7
ETHYLCELLULOSE	11.1
TRIETHYLCITRATE	4.5
	100.00

EXAMPLE 11

45 g of ketoprofen dissolved in 450 cc of methylene chloride were loaded onto 225 g of crosslinked β -cyclodextrin (Ciclodex - Chinoin, Budapest) kept under constant stirring in a sigma mixer. After homogenization of the pasty mass the swelling solvent was extracted by a vacuum pump at a residual pressure of 450-500 mbar. After evaporation and recovery of the methylene chloride the loaded product was collected and drying completed in a vacuum oven (1 hour at 30 °C). The 270 g of prepared product were then screened and homogenized by mixing. Colloidal silica (Aerosil 200, Degussa) and magnesium stearate were added to the final loaded product, which was then divided into flat tablets of 15 mm diameter weighing 500 mg. These tablets were then reduced to granules with a knife mill (or oscillating granulator). The 425-1000 μ m granulate fraction as removed by screening.

200 g of the granulate prepared as described above were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 525 g of solution of Povidone (Kollidon 25, BASF) in ethanol with added talc F.U. (anti-adhesion agent) and glycerin (plasticizer) under the following operating conditions: spraying pressure 1 bar, feed rate of coating suspension 4.5-6 g/min, inlet air temperature 30-34 °C, product temperature 28-30 °C, air volume during process 1.5-2.5 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume.

215 g of this coated granulate were suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, West Germany) and coated with 285 g of colloidal suspension of ethylcellulose (Aquacoat ECD-30 FMC) with added triethylcitrate (plasticizer) under the following operating conditions: spraying pressure 1-1.5 bar, feed rate of coating suspension 3.5-5.5 g/min, inlet air temperature 50-55 °C, product temperature 30-35 °C, air volume during process 1.5-2 m³/min. On termination of spraying, drying was carried out at the same inlet air temperature and volume. Percentage composition of final coated product:

Ketoprofen	12.35
Crosslinked β -cyclodextrin	61.8
Colloidal silica	0.37
Magnesium stearate	0.37
PVP K25	5.15
Glycerin	0.48
Ethylcellulose	14.98
	<u>4.51</u>
	100.00

EXAMPLE 12

293 g of diltiazem hydrochloride are activated by high-energy co-grinding with 147g of PVP Cl using a ball mill.

The duration of the grinding cycle is 2 hours at the maximum speed of the mill.

424 g of 2:1 co-ground diltiazem/PVP CL are granulated in a fluidized bed (Glatt GPCG1 W.G.) using a binding polymer granulating dispersion. 208 g of the obtained granulate are formulated as follows:

Granulated diltiazem	208 g
Magnesium stearate	4.5 g
Micronized talc	1 g
Avicel PH 102	<u>38 g</u>
	251.5 g

and the mixture is pressed using an automatic rotary press. The tablets obtained are granulated in a VIANI oscillating granulator through a screen of 1.3 mm mesh.

225 g of granulate prepared as described are suspended in a 4" Wurster column of a GPCG1 fluidised bed plant (Glatt, W.G.) and coated to the extent of 10% with 301.6 g of an alcoholic solution of Eudragit RS PM acrylic polymer (Röhm Pharma) using the following formulation for the coating:

Eudragit RS PM	22.5 g
Micronized talc	4.48 g
Citroflex 2	4.48 g
96% ethanol	<u>270.16 g</u>

This first coating is applied to the extent of 10% by weight of the granulate, under the following operating conditions:

atomization pressure	1 bar
feed rate of coating suspension	5.6 g/min
air inlet temperature	30 °C
product temperature	<u>25 °C</u>

230 g of the granulate previously coated with 10% of Eudragit RS PM are suspended in the previously used 4" Wurster column and coated with 182 g of a Eudragit NE 30D polymer suspension.

Film coating composition:

Eudragit NE 30D	76.64 g (23 dry)
Micronized talc	7 g
Water	<u>98.37 g</u>

The total coating is therefore 20%. On completion of the coating procedure, rapid drying is effected under the same air conditions. The thus coated granulate had the following percentage composition:

Diltiazem HCl	38.85
PVP CL	19.49
Eudragit NE 30D	14.68
Eudragit RS PM	7.80
Magnesium stearate	1.39
Micronized talc	4.55
Avicel PH 102	11.7
Citroflex 2	1.54
TOTAL	100.00

For purposes of comparison the following compositions were prepared by simply loading the medicament onto the swellable hydrophilic polymer but without coating with the polymer film.

EXAMPLE 13

332 g of sodium monofluorophosphate dissolved in 2000 g of demineralized water were loaded on 1660 g of crospovidone (Kollidon CL, BASF), previously mixed with 166 g of povidone (Kollidon 25, BASF), in a sigma mixer under continuous mixing. The homogenized mixture was dried in a fluidized bed (Glatt GPCG 1) for 2 hours at a temperature of 60-70°C and with an air velocity of 4-5 m/sec.

After sieving, the granular product having particle size 200-500 µm was suspended in a 4" Wurster column of a GPCG 1 fluidized bed plant (Glatt, West Germany) and coated with 140 g of a 10% povidone solution in ethanol 95% with added talc and glycerol under the following conditions: atomization pressure 1-1.5 bar; nozzle size 1 mm; feed rate of coating suspension 4-6 g/min; inlet air temperature 40-45°C; product temperature 25-30°C; flow of air 1.5-2 m³/min.

On termination of spraying, drying was carried out at the same inlet air temperature. The thus coated granular product had the following percentage composition:

Sodium monofluorophosphate	14.40
Kollidon CL	72
Kollidon 25	12.09
Talc	1.08
Glycerol	0.43
	100.00

EXAMPLE 14

210 g of the granulate previously coated as described in example 13 are suspended in a 4" Wurster column of a GPCG 1 fluidized bed plant (Glatt, West Germany) and coated with 1000 g of a 6% Ethylcellulose (NF 22, Hercules) in methylene chloride/ethanol 80/20 with added micronized talc and dibutyl sebacate under the following conditions: atomization pressure 1 bar; nozzle size 1.2 mm; feed rate 5-8 g/min; inlet air temperature 40-42°C; product temperature 28-30°C; flow of air 1.5-2 m³/min.

On termination of spraying, drying was carried out at the same inlet air temperature. The thus coated granular product had the following percentage composition:

Sodium monofluorophosphate	10.02
Kollidon CL	50.12
Kollidon 25	8.42
Glycerin	0.30
Talc	5.66
Ethylcellulose	19.60
Dibutyl sebacate	5.88
	<u>100.00</u>

EXAMPLE A

600 g of crospovidone (Kollidon CL, BASF) were loaded with 120 g of griseofulvin dissolved in 1.2 litres of methylene chloride in a chamber of a sigma mixer under continuous mixing. The thus swollen powder is dried in the same chamber at ambient temperature under a residual pressure of 450-500 mbar. Drying is completed in a vacuum oven for 1 hour at 30 °C.

% composition:

Griseofulvin	16.6
PVP CL	83.4
	<u>100.0</u>

EXAMPLE B

250 g of diacerein were activated by high-energy grinding with 250 g of crospovidone (Kollidon CL-M, BASF). 500 g of a mixture of excipients (30% lactose, 40% microcrystalline cellulose, 30% corn starch) were then added to the 500 g of co-ground product and the resultant mixture wet-granulated using a 5% hydroxypropyl cellulose solution in water as binder. The mixture was wet-screened and dried in a fluidized bed (GPCG1 Glatt, West Germany) under the following operating conditions: air inlet temperature 55 °C, air inlet volume 1-1.5 m³/min. The product was then dry-screened in an oscillating granulator.

% composition:

Diacerein	24.4
PVP CL	24.4
Cellulose	19.5
Corn starch	14.6
Lactose	14.6
Hydroxypropyl cellulose	2.5
	<u>100.00</u>

EXAMPLE C

45 g of nifedipine dissolved in 450 cc of methylene chloride were loaded onto 225 g of crospovidone (Kollidon CL-M, BASF) kept under constant stirring in a sigma mixer. After homogenization of the pasty mass the swelling solvent was extracted by a vacuum pump at a residual pressure of 450-500 mbar. After evaporation and recovery of the methylene chloride the loaded product was collected and drying completed in a vacuum oven (1 hour at 30 °C).

The 270 g of prepared product were returned to the mixing chamber of the sigma mixer and exposed to methylene chloride vapour for 24 hours. This operation was followed by drying in an oven, screening and homogenization by mixing the product. Colloidal silica (Aerosil 200, Degussa) was added to the final loaded product, which was then divided into flat tablets of 15 mm diameter weighing 500 mg and having a hardness of 7-10 Kp. These tablets were then reduced to granules with an oscillating granulator (or knife mill). The 425-1200 µm granulate fraction was removed by screening.

% composition:

Nifedipine	16.6
PVP CL	82.9
Colloidal silica	0.5
	<u>100.0</u>

EXAMPLE D

293 g of diltiazem hydrochloride are activated by high-energy co-grinding with 147g of PVP CL using a ball mill. The duration of the grinding cycle is 2 hours at the maximum speed of the mill.

% composition:

Diltiazem HCl	66.6
PVP CL	33.4
	<u>100.0</u>

Determination of dissolution rate

The dissolution data for the productions prepared by the process of this invention (Examples 1 to 14) are given in Tables 1-6. For comparison, each table also shows the dissolution rate data for the products prepared by simple loading onto the swellable hydrophilic polymer without subsequent coating with a polymer film (Examples A, B, C and D).

The method used for all the studied medicaments, with exception of medicament of example 14, was the U.S.P. XXI No. 2 method using the SOTAX apparatus at 37°C and a Beckman Du 65 spectrophotometer.

For the products containing griseofulvin 900 ml of pH 7.5 buffer were used with stirring at 150 r.p.m. The spectrophotometric reading of the suitably diluted samples was performed at $\alpha = 294$ nm.

For the products containing diacerein 900 ml of pH 5.5 buffer were used with stirring at 100 r.p.m. The spectrophotometric reading of the suitably diluted samples was performed at $\alpha = 255$ nm.

For the products containing nifedipine 900 ml of pH 7.5, pH 4.6 and pH 5.5 buffer with and without Tween 80 as surfactant were used with stirring at 150 r.p.m. The spectrophotometric reading of the suitably diluted samples was performed at $\alpha = 235$ nm.

For the products containing diltiazem 900 ml of pH 7.5, pH 5.5 and pH 1.2 buffer were used with stirring at 100 r.p.m. The spectrophotometric reading of the suitably diluted samples was performed at $\alpha = 233$ nm.

The dissolution rate of the product containing sodium monofluorophosphate (example 14) was determined by the method U.S.P. XXII No. 2 using the SOTAX apparatus at 37°C.

500 ml of deionized ultrapurified water with stirring at 100 r.p.m. were used.

The reading of the samples was performed by potentiometric route after enzymatic digestion for obtaining the transformation in fluoride ion and after correction of ionic force.

As can be seen from the data of Tables 1-6, for all the medicaments and all the coating polymers used, in every case there was a clearly more delayed and controlled dissolution rate for the products prepared by the process of this invention than for the analogous products prepared exclusively by loading onto the swellable hydrophilic polymer.

Table 4 also shows the release at different pH values for nifedipine from particles of crosslinked polyvinylpyrrolidone coated with acrylic polymer of pH-dependent solubility. It is evidently possible with the product of the present invention to obtain release rates which differ greatly with pH.

TABLE 1

Dissolution rate of products containing griseofulvin loaded onto crospovidone and coated with acrylic polymer:			
TIME	% GRISEOFULVIN RELEASED		
	Comparison preparation (EXAMPLE A)	Invention preparation (EXAMPLE 1)	Invention preparation (EXAMPLE 2)
15 min	47.6%	16.2%	22.2%
30 min	65.7%	26.3%	30.3%
60 min	83.8%	38.9%	41.5%
120 min		55.9%	54.2%
180 min		69.3%	68.5%
240 min		76.6%	74.0%
360 min		80.2%	
480 min		88.2%	81.2%
600 min		96.0%	85.6%
720 min			89.9%

TABLE 2

Dissolution rate of products containing diacerein loaded onto crospovidone and coated with acrylic polymer:					
TIME	% DIACEREIN RELEASED				
	Comparison preparation (EXAMPLE B)	Invention preparation (EXAMPLE 3)	Invention preparation (EXAMPLE 4)	Invention preparation (EXAMPLE 5)	Invention preparation (EXAMPLE 6)
15 min	83.4%	5.4%	3.3%	9.9%	3.5%
30 min	94.6%	7.2%	4.2%	18.3%	5.3%
60 min	100.7%	12.9%	4.9%	31.4%	12.9%
120 min		22.6%	7.9%	47.8%	32.4%
180 min		29.1%	10.8%	60.6%	51.0%
240 min		36.2%	12.7%	64.4%	66.6%
360 min		44.1%	15.9%	71.5%	81.3%
420 min		45.5%	17.0%	75.2%	90.4%
480 min		48.5%	19.8%	79.2%	93.0%
540 min		49.4%	21.2%	82.4%	
600 min		51.3%		83.6%	
720 min		58.2%			

TABLE 3

Dissolution rate of products containing nifedipine loaded onto crospovidone and coated with acrylic polymers and cellulose derivatives:					
TIME	% NIFEDIPINE RELEASED				
	Comparison preparation (EXAMPLE C)	Invention preparation (EXAMPLE 8)		Invention preparation (EXAMPLE 9)	Invention preparation (EXAMPLE 10)
	pH 7.5	pH 4.6	pH 7.5	pH 7.5 + 1% tween 80	PH 7.5 + 1% tween 80
15 min	64.8%		80.0%	12.1%	34.4%
30 min	87.5%	30.0%	98.9%	13.0%	49.4%
60 min	104.8%	33.0%		13.2%	54.3%
120 min		36.1%		15.5%	58.6%
180 min			105.0%	16.4%	61.2%
300 min			41.2%		71.0%
360 min				22.4%	
420 min			42.6%		75.1%

TABLE 4

Influence of pH on dissolution rate of products containing nifedipine loaded onto crospovidone and coated with acrylic polymer of pH-dependent solubility			
TIME	% NIFEDIPINE RELEASED		
	Comparison preparation (EXAMPLE C)	Invention preparation (EXAMPLE 7)	
	pH 7.5	pH 5.5	pH 7.5
15 min	64.8%	17.2%	62.3%
30 min	87.5%	29.0%	64.6%
60 min	104.8%	38.2%	90.5%
120 min		38.6%	108.0%

TABLE 5

Dissolution rate of products containing diltiazem hydrochloride loaded onto crospovidone and coated with polymers:		
TIME	% DILTIAZEM HCl RELEASED	
	Comparison preparation (EXAMPLE D)	Invention preparation (EXAMPLE 12)
1 min	86.9%	-
2 min	96.0%	-
3 min	96.8%	-
15 min		2.5%
60 min		3.2%
120 min		10.5%
240 min		25.7%
360 min		41.4%
480 min		61.0%
600 min		85.4%

TABLE 6

Dissolution rate of product containing sodium nonofluorophosphate (MFP) loaded onto crospovidone and coated with ethylcellulose		
TIME	% MFP RELEASED (EXAMPLE 14)	
60 min	57.83%	
120 min	74.77%	
240 min	83.06%	
480 min	94.29%	
12 h	99.70%	

Claims

1. A process for preparing therapeutic compositions with controlled release of medicaments, comprising the following stages:
 - 1) loading particles of at least one hydrophilic water-insoluble but water-swelling cross-linked polymer with a medicament, by swelling the cross-linked polymer with solutions of the medicament followed by drying, or by high-energy co-grinding;
 - 2) optionally size-enlarging the medicament-loaded particles by wet or dry granulation;
 - 3) coating the medicament-loaded particles obtained from stage 1 or the granules obtained from stage 2 by suspending them in an air stream, spraying with a solution of the coating polymer, and then drying.
2. The process as claimed in claim 1, wherein stage 1 is effected by any of the following methods:
 - 1a) dissolving the medicament in a solvent, spraying a volume of the solution so obtained onto a given amount of polymer and drying the product obtained;
 - 1b) dissolving the medicament in a solvent and suspending the cross-linked polymer in an excess of the solution obtained, stirring the suspension until the polymer particles have swollen, recovering the product and drying;
 - 1c) homogeneously mixing the medicament and the cross-linked polymer, both in powder form, and co-grinding them in a high-energy apparatus;
 - 1d) homogeneously mixing the medicament and the cross-linked polymer, both in powder form, and co-grinding them in a high-energy apparatus in which the grinding chamber is saturated with solvent vapour or subjected to a stream of vapour, the solvent being chosen from those able to swell the cross-linked polymer;

1e) the medicament and the cross-linked polymer, both in powder form, are homogeneously mixed and co-heated to the medicament melting-point until the medicament has been absorbed by the polymer.

- 5 3. The process as claimed in claim 1, wherein stage 3 is effected in a fluidized bed apparatus.
4. The process as claimed in claim 1, wherein the weight ratio of medicament to said cross-linked polymer is between 0,1 and 1000 parts by weight of medicament per 100 parts of polymer.
- 10 5. The process as claimed in claim 1, wherein the weight ratio of medicament to said cross-linked polymer is between 10 and 100 parts by weight of medicament per 100 parts of polymer.
6. The process as claimed in claim 1, wherein a mixture of cross-linked polymers is used.
- 15 7. The process as claimed in claim 1, wherein the cross-linked polymer is crospovidone.
8. The process as claimed in claim 1, wherein the cross-linked polymer is cross-linked β -cyclodextrin.
9. The process as claimed in claim 1, wherein the coating polymer consists of one or more linear polymers.
- 20 10. The process as claimed in claim 1, wherein the medicament is a poorly water-soluble one.
11. The process as claimed in claim 1, wherein the medicament is a water-soluble one.
- 25 12. The process as claimed in claim 1, wherein the loaded polymer particles obtained from stage 1 have a size of between 1 and 200 μm .
13. The process as claimed in claim 1, wherein the loaded polymer granules obtained from stage 2 have a size of between 100 and 1000 μm .
- 30 14. The process as claimed in claim 1, wherein the coated polymer particles have a size of between 10 and 1500 μm .
- 35 15. Controlled release compositions, obtainable by the process claimed in claim 1 to 14.

Patentansprüche

- 40 1. Verfahren zur Herstellung von therapeutischen Zusammensetzungen mit gesteuerter Freisetzung von Medikamenten, umfassend die folgenden Stufen:
 - 1) Beladen von Teilchen von zumindest einem hydrophilen, wasserunlöslichen, aber in Wasser quellbaren, vernetzten Polymer mit einem Medikament durch Quellen des vernetzten Polymers mit Lösungen des Medikamentes mit anschließendem Trocknen, oder durch Hochenergie-Covermahlen;
 - 2) wahlweises vergrößern der Größe der mit Medikament beladenen Teilchen durch Naß- oder Trockengranulierung;
 - 45 3) Beschichten der mit Medikament beladenen Teilchen, erhalten von Stufe 1 oder der Körnchen, erhalten von Stufe 2, durch Suspendieren dieser in einem Luftstrom, Sprühen mit einer Lösung des Beschichtungspolymers und anschließendes Trocknen.
- 50 2. Verfahren nach Anspruch 1, worin Stufe 1 durch eines der folgenden verfahren bewirkt wird:
 - 1a) Auflösen des Medikamentes in einem Lösungsmittel, Sprühen eines Volumens der so erhaltenen Lösung auf eine gegebene Menge des Polymers und Trocknen des erhaltenen Produktes;
 - 1b) Auflösen des Medikamentes in einem Lösungsmittel und Suspendieren des vernetzten Polymers in einem Überschuß der erhaltenen Lösung, Rühren der Suspension, bis die Polymerteilchen
 - 55 gequollen sind, Wiedergewinnen des Produktes und Trocknen;
 - 1c) homogenes vermischen des Medikamentes und des vernetzten Polymers, wobei beide in Pulverform vorliegen, und Covermahlen dieser in einer Hochenergieanlage;

- 1d) homogenes Vermischen des Medikamentes und des vernetzten Polymers, wobei beide in Pulverform vorliegen, und Covermahlen dieser in einer Hochenergieanlage, worin die Mahlkammer mit Lösungsmitteldampf gesättigt ist oder einem Dampfstrom unterworfen wird, wobei das Lösungsmittel von solchen ausgewählt ist, die das vernetzte Polymer quellen können,
- 5 1e) das Medikament und das vernetzte Polymer, die beide in Pulverform vorliegen, werden homogen vermischt und zu dem Medikamentschmelzpunkt coerhitzt, bis das Medikament durch das Polymer absorbiert ist.
3. Verfahren nach Anspruch 1,
10 worin Stufe 3 in einer Fließbettanlage durchgeführt wird.
4. Verfahren nach Anspruch 1,
worin das Gewichtsverhältnis des Medikamentes zu dem vernetzten Polymer zwischen 0,1 und 1000 Gew.Teilen Medikament pro 100 Teile Polymer ist.
- 15 5. Verfahren nach Anspruch 1,
worin das Gewichtsverhältnis des Medikamentes zu dem vernetzten Polymer zwischen 10 und 100 Gew.Teilen Medikament pro 100 Teile Polymer ist.
- 20 6. Verfahren nach Anspruch 1,
worin eine Mischung an vernetztem Polymer verwendet wird.
7. Verfahren nach Anspruch 1,
worin das vernetzte Polymer Crospovidon ist.
- 25 8. Verfahren nach Anspruch 1,
worin das vernetzte Polymer ein vernetztes β -Cyclodextrin ist.
9. Verfahren nach Anspruch 1,
30 worin das Beschichtungspolmer aus einem oder mehreren linearen Polymeren besteht.
10. Verfahren nach Anspruch 1,
worin das Medikament gering wasserlöslich ist.
- 35 11. Verfahren nach Anspruch 1,
worin das Medikament wasserlöslich ist.
12. Verfahren nach Anspruch 1,
40 worin die beladenen Polymerteilchen, die von Stufe 1 erhalten werden, eine Größe zwischen 1 und 200 μm haben.
13. Verfahren nach Anspruch 1,
worin die beladenen Polymerteilchen, die von Stufe 2 erhalten werden, eine Größe zwischen 100 und 1000 μm haben.
- 45 14. Verfahren nach Anspruch 1,
worin die beschichteten Polymerteilchen eine Größe zwischen 10 und 1500 μm haben.
15. Zusammensetzungen mit gesteuerter Freisetzung,
50 erhältlich durch das Verfahren nach den Ansprüchen 1 bis 14.

Revendications

1. Un procédé de préparation de compositions thérapeutiques présentant une libération contrôlée des médicaments, comprenant les étapes suivantes:
- 55 1) chargement de particules constituées d'au moins un polymère réticulé hydrophile, insoluble dans l'eau mais gonflant dans l'eau, avec un médicament, par gonflement du polymère réticulé avec des solutions de médicament, suivi d'une étape de séchage, ou par cobroyage à puissance élevée;

2) éventuellement, augmentation de la taille des particules chargées de médicament par granulation par voie sèche ou par voie humide;

3) revêtement des particules chargées de médicament obtenues dans l'étape 1) ou des granulés obtenus dans l'étape 2) par mise en suspension de ces derniers dans un courant d'air, pulvérisation de ces derniers avec une solution du polymère de revêtement, puis séchage.

2. Le procédé selon la revendication 1, dans lequel l'étape 1) est mise en oeuvre par l'une quelconque des méthodes suivantes:

1a) dissolution du médicament dans un solvant, pulvérisation d'un volume de la solution ainsi obtenue sur une quantité donnée du polymère et séchage du produit obtenu;

1b) dissolution du médicament dans un solvant et mise en suspension du polymère réticulé dans un excès de la solution obtenue, agitation de la suspension jusqu'à ce que les particules de polymère aient gonflé, récupération du produit et séchage;

1c) mélange homogène du médicament et du polymère réticulé, les deux produits étant sous une forme pulvérulente, et cobroyage de ces derniers dans un appareil à puissance élevée;

1d) mélange homogène du médicament et du polymère réticulé, les deux produits étant sous forme pulvérulente, et cobroyage de ces derniers dans un appareil à puissance élevée dans lequel la chambre de broyage est saturée avec de la vapeur de solvant ou soumise à un courant de vapeur, le solvant étant choisi parmi ceux qui sont capables de faire gonfler le polymère réticulé;

1e) le médicament et le polymère réticulé, tous les deux sous forme pulvérulente, sont mélangés de façon homogène et co-chauffés au point de fusion du médicament, jusqu'à ce que le médicament ait été absorbé par le polymère.

3. Le procédé selon la revendication 1, dans lequel l'étape 3 est mise en oeuvre dans un appareil à lit fluidisé.

4. Le procédé selon la revendication 1, dans lequel le rapport pondéral médicament/polymère réticulé précité est compris entre 0,1 et 1000 parties en poids de médicament pour 100 parties de polymère.

5. Le procédé selon la revendication 1, dans lequel le rapport pondéral médicament/polymère réticulé précité est compris entre 10 et 100 parties en poids de médicament pour 100 parties de polymère.

6. Le procédé selon la revendication 1, dans lequel un mélange de polymères réticulés est utilisé.

7. Le procédé selon la revendication 1, dans lequel le polymère réticulé correspond au crospovidone.

8. Le procédé selon la revendication 1, dans lequel le polymère réticulé correspond à de la β -cyclodextrine réticulée.

9. Le procédé selon la revendication 1, dans lequel le polymère de revêtement consiste en un ou plusieurs polymères linéaires.

10. Le procédé selon la revendication 1, dans lequel le médicament est un médicament faiblement soluble dans l'eau.

11. Le procédé selon la revendication 1, dans lequel le médicament est un médicament hydrosoluble.

12. Le procédé selon la revendication 1, dans lequel les particules de polymère chargé obtenues à partir de l'étape 1 présentent une dimension comprise entre 1 et 200 microns.

13. Le procédé selon la revendication 1, dans lequel les granulés de polymère chargé obtenus à partir de l'étape 2, présentent une dimension comprise entre 100 et 1000 microns.

14. Le procédé selon la revendication 1, dans lequel les particules de polymère chargé présentent une dimension comprise entre 10 et 1500 microns.

15. Composition à libération contrôlée, susceptible d'être obtenue par les procédés selon les revendications 1 à 14.